VESSEL PARTICULARS (FORM C) LPG/C GAS SINCERITY (last updated 27/05/2010)

Specifications of the vessel and the gas installation which are representations by the Owners.

 (A) VESSEL'S CHA PREAMBLE Name Owner Flag Build Date on Service Class 	AR/ : : : :	ACTERISTICS GAS SINCERITY SOLEIL TRUST INC PANAMA WATANABE SHIPB 13 JULY 2000 Lloyd's	2. SUILDING CO.,LTD.			
GRT International	:	3818 T	Suez Panama	:		4225.14 T 3266 T
NRT International	:	1146	Suez Panama	:		
Is vessel build according	g to		USCG regulations? RINA regulations? Japanese regulation?	::	Yes N/A N/A	
Has vessel received			USCG approval? RINA approval?	:	Yes N/A	

99.97 M
94.70 M
16.80 M
7.50 M
5.364 M corresponding to Summer DWT = 3847.11 MT
N/A M corresponding to Multiple DWT = N/A

Estimated draft with full cargo and full bunkers are as follows.

Product	Draft Fore' (m)	Draft Aft' (m)	Draft Mean (m)	Corresponding Deadweight (t)
Propane (98%)	3.72	5.93	4.83	5539.97
Butadiene (98%)	4.20	6.17	5.19	6026.59
VCM (98%)	4.29	6.39	5.34	6234.05

Propeller immersion :

At draft Aft 5.93 m correspond. :109.71% At draft Aft 6.17 m correspond. : 116.76% At draft Aft 6.39 m correspond. : 123.24%

COMMUNICATION EQUI	PMENT		
Call letter		:	H3JE
Radio Station normally wa	tched	:	GMDSS
Radio MF/HF NBDP		:	FITTED
Radio MF/HFTEL/DSC		:	FITTED
VHF		:	FITTED
Satellite Communication	Inmarsat 'C'	:	4354225510
	Inmarsat 'Flt 33'	:	764818872/73
		:	
		:	

MACHINERY

Main Engine x 1 .	Type and make:Service power:No of CylindersCyl Bore x StrokeGrade of fuel used:	AKASAKA-MITSUBISHI UE DIESEL ENGINE 6UEC37LA 4200 PS x 210 RPM 6 370 X 880 380 CST @ 50 deg.C
Auxiliaries	Type and make (Electrical) (Mechanical) Grade of fuel used No off	YANMAR SI65L – UN 265 KW 400 KVA x 445V , 60HZ x 2 SETS Diesel Oil
Emergency Gen	Type No off	YANMAR
Bow Thruster	Type : Power:	KAMOME TCA-60MA
Boiler	Туре	WATER TUBE
	Evaporation Max Design Pressure	538 kg/h 0.7 Mpa
	Feed Water Temp No off	85 ~ 90 deg.C. 1
Exhaust Economiser	Туре	FORCE CICULATING TYPE MULTITUDINOUS TUBE (FINE TUBE)
	Evaporation No off	400 kg/h
Air Compressors (Main)	Type / Capacity	VERTICAL 2-STAGE / 53.0m3/h (Direct Drive)
(-)	No off	2 sets
Air Compressors (Emergency)	Туре	DIESEL DRIVEN / 6.3 m3/h
(No off	1 SET
Fuel Oil Purifier	Type No off	SELF JECTOR (SJ-15F) SERIES 3 SETS

Lub Oil Purifier	Capacity			FO- (C) – 1299 D.O.(A) – 4350 SELE JECTOR	l/h l/h (S L15E) SERIES	
	No off Capacity			1 INIT 1700~ 2850 L/H	(30-131) SERIES	
Evaporator	Type Capacity			WM-10M 10 T/DAY		
Fresh Water Sterilizer	Туре			USS-1K		
	Capacity			1000 L/H		
Fresh Water Mineraliser	Type / Ca	pacity		N/A		
Waste Oil Incinerator (IMO MEPC 76 (40))	Туре			BGW-20N		
	Capacity			WASTE OIL-25	.0KG/H / SOLID WASTE 20 KG/H	
Oily Water Separator	Type Capacity			USC – 10 1 m3/H		
Sewage Treatment	Туре			SBT-25		
	Capacity			25 PERSON / DAY		
Hot Water Set (Calorifier unit)	No off			1 SET / CFL-20	00-5	
Steering Gear	Type Duty Capa	acity		RV21-017(ELI 170 KN-M	ECTRO HYDRAULIC)	
	Hydraulic unit	pump		LVP017-210RC AXIAL PISTON	DL (2 SETS)(BENT AXIS TYPE PUMP)	
Speed I Up to and Beaufort Sc About 13.5 KNOTS	ale 4 Douglas Ballast/Lac	s Sea sta len	ate 3			
CONSUMPTION/ DAY At Sea						
Main Engine	HFO	About	12.0	MT/Day MT/Day	Ballast/Laden	
In Port	MGO	About	1.0	MT/Day	Idle	

MGO	About	1.0	MT/Day
MGO	About	1.0	MT/Day
MGO	About	2.2	MT/Day

Discharging

Permanent bunker capacity (100%)

HFO	:	About 569.86 m3
Diesel	:	About 111.83 m3
Fresh Water	:	163.16m3

(B) CARGO INSTALLATIONS

1.	Transportable products and respective quantities, calculated in accordance with IMO - maximum
	filling formula. (Tonnes)

	100% (CBM)	98% (CBM)		
NO.1 CARGO TANK	2064.486	2023.196		
NO.2 CARGO TANK	2064.492	2023.202		
TOTAL				
	SPSV	Ref. Temp. (deg.	Density at	Corresponding
	(bar g)	C.)	(Ref. Temp.)	Quantity (MT)
Propane	17.65	45.0	0.459	1857.00
Propylene	17.65	45.0	0.470	1901.80
B/P Mixture	17.65	45.0	0.487	1810.369
I-Butane	17.65	45.0	0.526	2217.4
N-Butane	17.65	45.0	0.548	2217.4
Butylene	17.65	45.0	0.565	2121.348
Butadiene	17.65	45.0	0.588	2379.2
V.C.M.	17.65	45.0	0.872	3000.0
Isoprene	17.65	45.0	0.656	N/A
Pentane	17.65	45.0	0.600	N/A
Pentene	17.65	45.0	0.611	N/A

Note(1): In case of USCG, propylene, propane and B/P mixtures are not to be carried except the vapour pressure of B/P mixtures is not more than 12.75 bar g, 13.0 kg/cm² @ 45 °C Note(2): On and after, the pressure value in parentheses is shown as a conversion value Mixing ratio of above mentioned B/P mixtures is as follows: Butane 35 wt% and propane 65 wt%

2. Other transportable products N/A

	SPSV	Ref. Temp. (°C.)	Density at Ref. Temp.	Corresponding Quantity (MT)
Raffinate 1				
Raffinate 2				
C4				

3. TANKS

3.1	Design pressure (Vapour) – BV-IGC	:	17.65 bar g (1.765 MPag)
	- USCG	:	12.75 bar g (1.275 MPag)
3.2	Valve setting	:	17.65 bar g (1.765 MPag) / 12.75 bar g
			(1.275 MPag)
3.3	Maximum vacuum obtainable	:	Atmospheric
3.5	Maximum temperature acceptable	:	45 ℃
3.6	Minimum temperature acceptable	:	℃ 0

4. LC	DADING RATE (TONS/HOUR) – For Full C	Cargo	Parce	ls
Ex-atn	nospheric storage with gas : 1 tar	٦k	:	204 tons/h Butane 0-30 deg.C
Return	n 2 tar	nks	:	
Remai	rks:			
* Base	ed on maximum velocity of 6.5 metres/sec e	except	VCM,	and 4.0 meters/sec for VCM
in th	e liquid piping.			2
* If car	go temperature is less than 0 °C, shore he	ater to	be us	ed. If ship heater used, max rate is 190 m 3
per	hour.			
* Load	ling by shore pump only, proper size gas re	eturn li	ne to b	e connected
* Subje	ect to both ship and shore tanks being unde	er favo	ourable	conditions
5. CA	ARGO PUMPS			
5.1	Туре	:	2 fixed	l deep well
	Make	:	Teikoł	ku Machinery Works
	How many	:	1 pum	p each
	Maximum specific gravity	:	0.948	
5.2	Capacity (CMB/Hour)	:	300 m3	/h(SG.0674) (LPG)110 mtrs / 250 m3h(SG.0.944)
			(VCM)	120 mtrs
	I wo speed or variable speed	:	One s	peed
	Rated kW (each)			
	Working pressure maximum	:		
5.0	Location		Tonk	
5.3	Domanualla	•		α 2
	Removable	:	NA	
5.4	Booster pumps	:	N/A	
	Туре	:	N/A	
	Maker	:	N/A	
5 5	Capacity (CMP/Hour)		N/A	
5.5	Working process	÷	N/Λ	
	working pressure	-	IN/A	
5.6	Location	:	N/A	
5.7	lime to discharge a full liquid cargo usi	ing all	pumps	s against back pressure at pump
	1 bar	:	about	11 hours for LPG
	5 bars	:	about	20hours for LPG
	10 bars	:		
5.8	Nominal back pressure when working	:	about	1 bar
	In series corresponding head		N/A	
	Maximum back pressure		about	5 bar
	Nominal pressure at rail (propane)	÷	about	13 bar at 20 degree C of cargo temperature
5.9	What amount of cargo remains in tanks	s after	compl	etion pumping before stripping:
	- liquid	:	about	per one tank /N/A
	- vapour	:	about	ton per one tank for LPG N/A
6. ST	RIPPING			
6.1	Stripping system. if anv	:	N/A	
	- FT	-		
~ ~	_			

: 26.48 bar g (2.648 MPag)

6.2 Time required to remove all traces of liquid cargo as stated in 5.9 for:

Form 'C' – TBA

3.7

Hydrostatic Test Pressure

	- LPG :	about hours / N/A
7. CAR 7.1	GO COMPRESSORS Type : Make : How many : Piston displacement Rated Kw Stroke Max discharge pressure Pressure differential	Reciprocated, Oil Free TANABE PNEUMATIC MACHINERY CO. 2 37KW 177.8 MM 19.62 BAR
7.0	No of Revolutions	540 RPM
7.2	Are compressors on free :	res
7.4	State time to bring full cargo of butane : to atmospheric pressure from	
8. INER 8.1	T GAS SYSTEM / N2 GENERATORDoes the vessel use inert gas?If so, state utilization and quantities	N/A N/A N/A
8.2	Can the vessel produce inert gas? : If so, state type and composition of gas proc	N/A Juce: N/A
	Discharge Capacity	
8.3	Maximum production obtainable	N/A
8.4	NOTE:- Above quantities obtained at engine State if there are storage facilities for inert g - Size : - Pressure :	e room temperature 45° C as onboard: N/A N/A N/A
8.5	State if any shore supply of nitrogen may be - for what purpose : - what quantities :	required: : Yes Gas Free/ DD/Change of Cargo TBA
9. GAS 9.1	FREEING State method used giving all details :	Nitrogen Plant / Fans
9.2	State time required including stripping :	ТВА
10. CHA	ANGING GRADE	

10.1 From completion discharge of cargo Propane, time required in hours and inert gas in CBM required to reach a tank and gas installation atmosphere of less than 100 ppm of Propane in Vapour phase.

Time required: TBA

10.2	Can this operation be carried out a	:	NO		
10.3	Can the ship measure the number	:	YES		
10.4	Has vessel deck tank for changing	coling operations?	:	NO	
10.5	Deck tanks Capacity Purpose	:	N/A N/A N/A		
11. CO	OLING BEFORE LOADING	:	N/A		
12. CA	RGO HEATER				
12.1	Туре	:	S-321 / KL33-SR		
12.2	Inside Diameter		276 MM		
12.3	Overall length		4746 MM		
12.4	Cargo flow rate		190 M3/H		
12.5	Min Inlet Temp		LESS THAN 0 DE	EG.	
12.6	Min Outlet Temp		+ 2 DEG		
12.7	Required Sea water Capacity		500 M3/H		
12.8	Design Pressure		1.96 MPA / SHEL	L SI	DE
12.9	Hydrostatic Test Pressure		2.94 MPA / SHEI	LL SI	DE
12.10	Tightness Test Pressure		2.16 MPA / SHEI	LL SI	DE

12.0 State discharging rate for propane to be brought from atmospheric pressure Loading rate for Propane - ° C / 0° C: **about 150** Mt/hr

13. CARGO VAPORIZER

In case vapour gas is needed to feed compressors, can vessel produce its own if no shore available:

NIL

14. RE 14.1	FRIGERATING APPARATUSNAIs it independent of cargo?:Is so, state cooling agents:	4 A A		
14.2	What minimum temperature can be maintained		:	NA
14.3	What time required at sea to lower by 1°C the fu	ull cargo of	:	NA

15. MEASURING APPARATUS

What gauges on board?	ONE FLOAT GAUGE WITH REMOTE FIXED IN EACH TANK AND 5 SLIP TUBES TYPE LEVEL GAUGE IN EACH TANK.
Type : Location :	LOCATION OF INDICATION AT BOTH ON TANK DOME AND CARGO MONITORING IN CARGO CONTROL ROOM.

16. SAMPLES

Form 'C' – TBA

16.1	State how tank atmosphere samples can be taken and where from? MID ,TOP.BOTTOM. Line.					
	Standard of fitting?	: 3/8 INCHES COUPLING				
16.2	Same question for cargo	: TBA				
16.3	Are sample bottles available on board?	? : No				
17. CAF 17.1	RGO LINES Is ship fitted with a port and starboard c	cargo manifold? : Yes				
17.2	Position of cargo manifold - distance from stern (AP) (S / P) - distance form stem (FP) (S / P) - height above deck - distance from ship's rail - underside keel to manifold	52.76 M 47.21 M 1.05 m for Liquid manifold 2.20 M 7.50 M				
17.3	Liquid line - flange-size - type	: 8 in. : ANSI / # 900				
	Gas line - flange-size - type	: 6 in. : ANSI / # 900				
17.4	What reducers on board? For Liquid line (low temperature)	: 8/6 , 8/5,8/4,8/3 (INCHES)				
	For Vapor line (normal temp.)	6/5,4/5,3/5(INCHES)				
17.5	ls ship fitted with stern discharge? - Liquid line - diameter - flange – size - type	No : N/A : N/A : N/A				
18. HOS	ES Are serviceable hoses available on boa	ard? : YES				
18.1	Length Diameter Flange-size Type Bending radius	2 SETS 50 FT. 4 INCHES / 2 INCHES 4" / 2" N/A N/A				
18.2	Minimum temperature acceptable Maximum pressure acceptable	: 0 DEG.CENT : 350 PSI				
18.3	For what products are hoses suitable?	:				

19. DERRICKS

- Hose cranes	:	Yes
- Where situated - Lifting capacity	:	3.5 Tons
- Working radius	:	12 M

20. SPECIAL FACILITIES

20.1	How many grades can be segregated?	:	No Segregation/ loading.	1	common	line
20.2	How many cooled?	:	N/A			
20.3	Can vessel sail with slack cargo tanks?	:	Yes			